

## Preparation and kinetic analysis of $\text{Li}_4\text{SiO}_4$ sorbents with different silicon sources for high temperature $\text{CO}_2$ capture

SHAN ShaoYun, JIA QingMing, JIANG LiHong, LI QinChao, WANG YaMing & PENG JinHui\*

Kunming University of Science and Technology, Kunming 650093, China

Received January 10, 2012; accepted February 16, 2012; published online May 6, 2012

Using diatomite and analytical pure  $\text{SiO}_2$  as silicon sources,  $\text{Li}_4\text{SiO}_4$  sorbents for high temperature  $\text{CO}_2$  capture were prepared through solid-state reaction method. Phase composition was analyzed by X-ray diffraction, and the  $\text{CO}_2$  absorption capacity and adsorption-desorption performance were studied by the simultaneous thermal thermogravimetric analyzer (TG-DSC). The results showed that silicon source had an important influence on  $\text{CO}_2$  absorption properties. The kinetic parameters for the chemisorption and diffusion processes were obtained by the isothermal study for different silicon sources. The results showed that the activation energies for these two processes were estimated to be 105.427 and 35.928 kJ/mol for the sample with analytical pure  $\text{SiO}_2$  (AS). While for the sample with diatomite (DS), the activation energies for these two processes were estimated to be 78.500 and 20.439 kJ/mol, respectively.

**kinetic, silicon sources, lithium silicate,  $\text{CO}_2$  capture**

**Citation:** Shan S Y, Jia Q M, Jiang L H, et al. Preparation and kinetic analysis of  $\text{Li}_4\text{SiO}_4$  sorbents with different silicon sources for high temperature  $\text{CO}_2$  capture. *Chin Sci Bull*, 2012, 57: 2475–2479, doi: 10.1007/s11434-012-5188-x

The increasing  $\text{CO}_2$  concentration in the atmosphere due to fossil fuel burning has been considered as a major contributor to the global warming. So the separation, recovery and storage/utilization of  $\text{CO}_2$  have attracted considerable attention in recent years.  $\text{CO}_2$  can be removed from flue gas and waste gas streams by various methods such as membrane separation, wet absorption, and dry absorption [1–4]. However, these methods need to consume a lot of energy. Hence, the materials with high  $\text{CO}_2$  capture capacity at high temperature are desirable.

In recent years, the development of regenerable sorbents for high temperature  $\text{CO}_2$  capture has received increasing attention [5–7]. Compared with other sorbents,  $\text{Li}_4\text{SiO}_4$  has the better  $\text{CO}_2$  absorption properties over a wide range of temperature and  $\text{CO}_2$  concentration [8,9]. In order to study the absorption mechanism of  $\text{Li}_4\text{SiO}_4$  materials, some researchers made some kinetic study about  $\text{Li}_4\text{SiO}_4$  materials [10]. However, kinetic study about different silicon sources

has not been reported.

In this paper, we firstly developed novel low-cost  $\text{Li}_4\text{SiO}_4$  sorbents for high temperature  $\text{CO}_2$  capture using diatomite as silicon source. The effect of different silicon sources on the absorption capacity was investigated by studying their kinetic characteristics. In the following paper, DS and AS stand for diatomite and analytical pure  $\text{SiO}_2$ , respectively.

### 1 Experimental

Diatomite (75% $\text{SiO}_2$ , C.R., Shanghai Fengxian Reagent Co. Ltd., China) and  $\text{SiO}_2$  (99%, A.R., Traditional China Medicine Chemical Reagent Co. Ltd., China) were used as silicon sources. The properties for diatomite are shown in Table 1.  $\text{Li}_2\text{CO}_3$  (97%, A.R., Tianjin Fengchuan Chemical Reagent Co. Ltd., China) was used as the starting powders.  $\text{Li}_4\text{SiO}_4$  materials were synthesized according to reaction (1) at 700°C for 2 h.

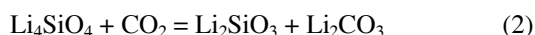
\*Corresponding author (email: Jhpeng@kmust.edu.cn)

**Table 1** Diatomite composition analysis

Compostion	SiO <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub>	Fe <sub>2</sub> O <sub>3</sub>	CaO	K <sub>2</sub> O	Loss	Others
Content (wt%)	75.26	14.33	2.31	1.02	1.56	4.35	1.17



Crystalline phases were identified by XRD (D8ADVANCE, Germany) analysis. The absorption properties of Li<sub>4</sub>SiO<sub>4</sub> materials with different silicon sources were investigated into the gas mixture (50 mL/min N<sub>2</sub> and 50 mL/min CO<sub>2</sub>) by TG-DSC (STA 449 F3, Netch Co. Ltd., Germany). The absorption reaction is



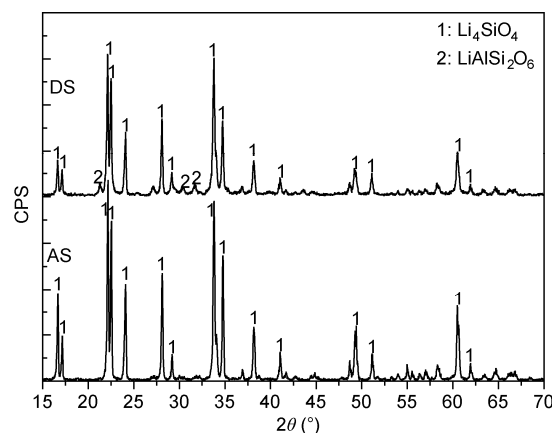
As seen from reaction (2), the theoretical absorption capacity of Li<sub>4</sub>SiO<sub>4</sub> is 36.7 wt%.

## 2 Results and discussion

### 2.1 Phase composition and microstructure of Li<sub>4</sub>SiO<sub>4</sub> sorbents

Figure 1 shows the diffractograms of Li<sub>4</sub>SiO<sub>4</sub> sorbents with different silicon sources prepared at 700°C for 2 h. As shown in Figure 1, Li<sub>4</sub>SiO<sub>4</sub> phase with  $a=5.30$  Å,  $b=6.32$  Å,  $c=5.45$  Å (JCPDS: 24-0650) was the main phase for the sample with DS and AS, which indicated that the reaction had happened completely according to reaction (1). While a small quantity of LiAlSi<sub>2</sub>O<sub>6</sub> phase (JCPDS: 33-0786) was observed for the sample with DS. The occurrence of LiAlSi<sub>2</sub>O<sub>6</sub> phase was resulted from the reaction between Al<sub>2</sub>O<sub>3</sub> phase coming from diatomite and Li<sub>2</sub>CO<sub>3</sub>. Different lithium aluminates have different absorption properties for CO<sub>2</sub>. LiAlO<sub>2</sub> did not seem to have good absorption properties for CO<sub>2</sub>, and Li<sub>5</sub>AlO<sub>4</sub> showed excellent behavior as a possible CO<sub>2</sub> captor [11]. However, the absorption properties of LiAlSi<sub>2</sub>O<sub>6</sub> for CO<sub>2</sub> are not known.

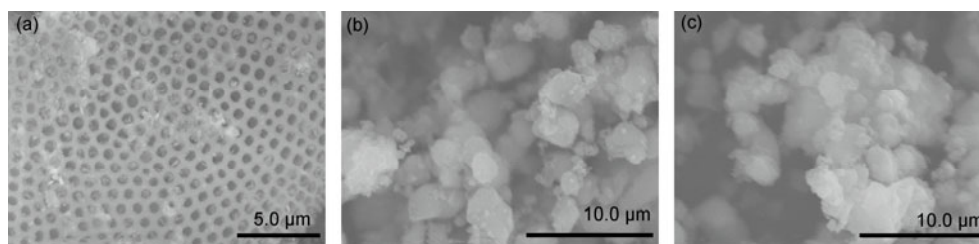
Figure 2 shows the microstructure of diatomite and the Li<sub>4</sub>SiO<sub>4</sub> sorbents with DS and AS. Seen from Figure 2(a), diatomite had rich pore structure and uniform pore distribution with the pore size of 0.5–1.0 μm. Seen from Figure 2(c), the sample with AS was mainly composed of some small spherical particles and a portion of large polygonal particles. Figure 2(b) shows that the sample with DS showed more

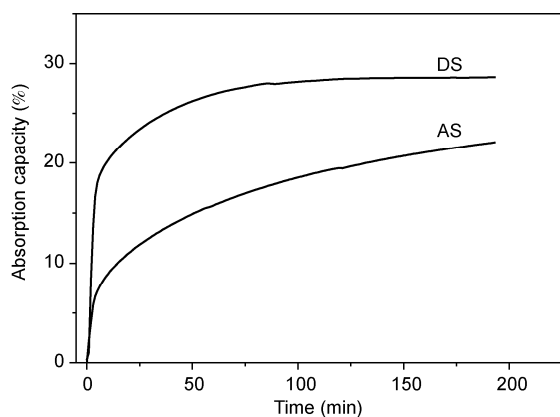
**Figure 1** XRD patterns of Li<sub>4</sub>SiO<sub>4</sub> sorbents with different silicon sources.

uniform microstructure, which was mainly composed of homogenous spherical particles with a particle size of about 1–3 μm. Obviously, the microstructure of the Li<sub>4</sub>SiO<sub>4</sub> with DS did not inherit that of diatomite, but the structure of silicon source had an important influence on the microstructure of the final Li<sub>4</sub>SiO<sub>4</sub> sorbents. The specific surface areas for the sample with DS and AS under the same preparation condition are 1.75 and 1.15 m<sup>2</sup>/g, respectively.

### 2.2 Effect of different silicon sources on absorption properties

Figure 3 shows the effect of different silicon sources on absorption capacity. As shown in Figure 3, the sample with DS had higher absorption capacity than that with AS at the same retaining time. The sample with DS had much quicker absorption rate before 10 min, and the absorption capacity of the sample with DS was almost twice as high as that of the sample with AS at 10 min. In addition, the absorption reaction reached equilibrium at 80 min for the sample with DS, but the sample with AS did not still reach equilibrium until 200 min. The maximum absorption capacity (28.62 wt%) for the sample with DS, being 78% of the theoretical absorption capacity, was higher than that (22.08 wt%) for

**Figure 2** SEM images of diatomite (a), the Li<sub>4</sub>SiO<sub>4</sub> sorbents with DS (b) and AS (c).



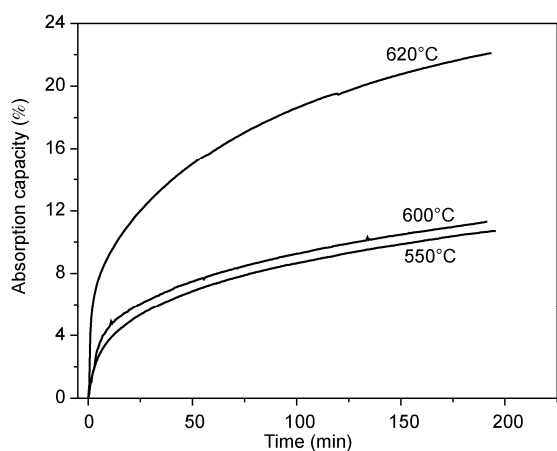
**Figure 3** Isotherms of  $\text{Li}_4\text{SiO}_4$  materials with different silicon sources at  $620^\circ\text{C}$ .

the sample with AS, which probably resulted from the larger specific surface area and more uniform microstructure for the sample with DS. Besides this, the results were also explained by the following kinetic analysis.

### 2.3 Kinetic analysis for $\text{Li}_4\text{SiO}_4$ sorbents with different silicon sources

Figure 4 shows the isothermal graphs of  $\text{Li}_4\text{SiO}_4$  materials with AS at different temperatures. As shown in Figure 4, the absorption capacity and the absorption rate increased with the absorption temperature. At  $550^\circ\text{C}$  or  $600^\circ\text{C}$ ,  $\text{Li}_4\text{SiO}_4$  materials only absorbed a small quantity of  $\text{CO}_2$  (about 10 wt%) at 200 min, while the  $\text{CO}_2$  absorption capacity reached 22.11 wt% at  $620^\circ\text{C}$  at 200 min.

In order to obtain some kinetic information about the  $\text{CO}_2$  absorption, some isothermal analyses were performed at different temperatures into the mixture gas (50 mL/min  $\text{N}_2$  and 50 mL/min  $\text{CO}_2$ ) (Figure 4). Seen from Figure 4, three absorption curves presented similar behaviors, and the data was fitted according to a double exponential model:  $y = A\exp(-k_1x) + B\exp(-k_2x) + C$ , where  $y$  represents absorption



**Figure 4** Isotherms of  $\text{Li}_4\text{SiO}_4$  materials with AS.

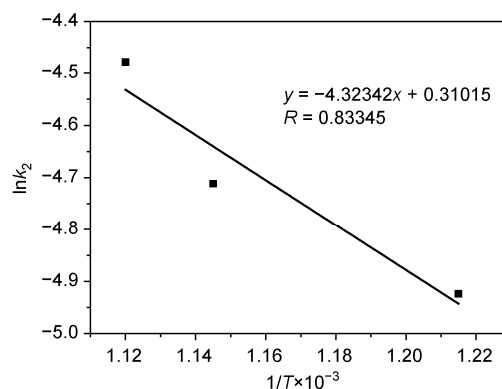
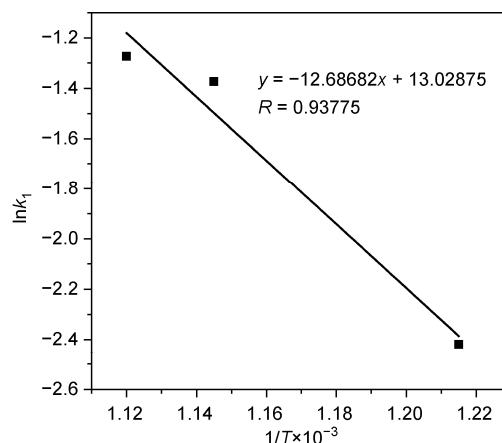
capacity,  $x$  is absorption time,  $k_1$  and  $k_2$  are the exponential constants, and  $A$ ,  $B$ , and  $C$  are the pre-exponential factors. The kinetic parameters obtained at three temperatures are shown in Table 2. As can be seen,  $k_1$  (chemisorption) values are about 10 times higher than those of  $k_2$  (diffusion), indicating that the diffusion is the limiting step of the total reaction. For a model of these characteristics, the gradients of these best fit lines usually confirm to the Arrhenius equation, so that

$$k = k_0 \exp\left(-\frac{E}{R_g T}\right),$$

where  $k$  is the reaction rate constant,  $k_0$  is the pre-exponential factor,  $E$  is the activation energy,  $R_g$  is the gas constant, and  $T$  is absolute temperature. Figure 5 shows the plots of  $\ln k$  versus  $1/T$ . The curves obviously show a linear trend for

**Table 2** Kinetic parameters obtained from the experimental data fitted to a double exponential model for the sample with AS

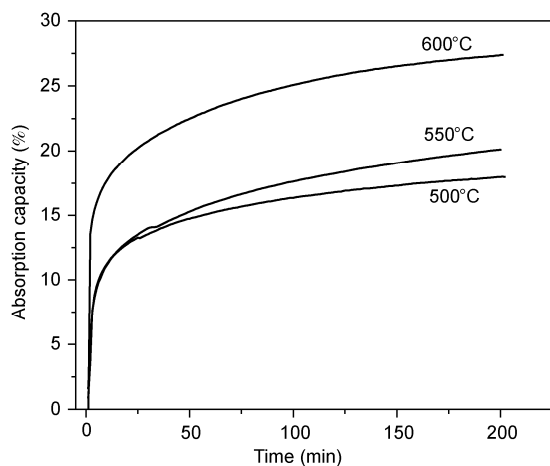
$T$ ( $^\circ\text{C}$ )	$k_1$ (1/s)	$k_2$ (1/s)	$R$
550	0.08905	0.00727	0.99964
600	0.25336	0.00899	0.99869
620	0.28016	0.01134	0.99855



**Figure 5** Plots of  $\ln k$  versus  $1/T$  for chemisorption ( $k_1$ ) and diffusion ( $k_2$ ) on  $\text{Li}_4\text{SiO}_4$  with AS.

both chemisorption process and diffusion process. Hence, the activation energies for the chemisorption and diffusion processes were estimated to be 105.427 and 35.928 kJ/mol, respectively. As can be seen, the activation energy of the chemisorption process is almost three times as high as that of the diffusion process, which showed that the chemisorption process was more dependent on the temperature.

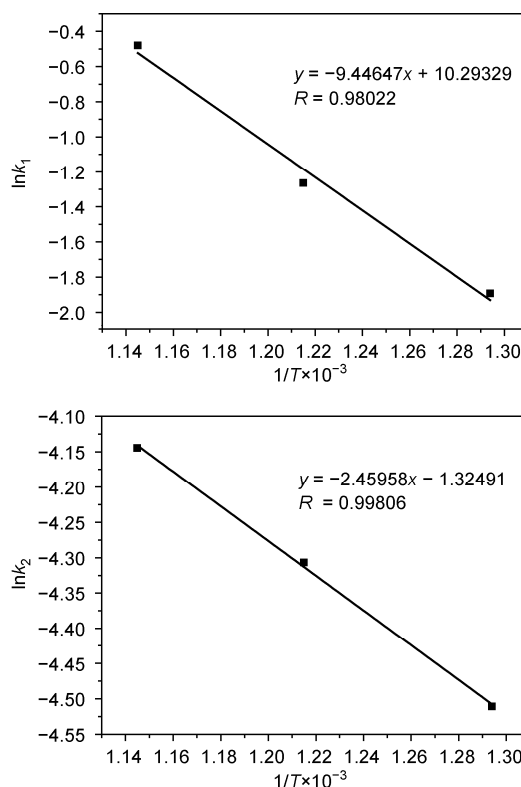
In order to analyze the effect of silicon source on the kinetic reaction, the  $\text{Li}_4\text{SiO}_4$  with DS was studied under the same conditions. Figure 6 shows the isothermal graphs of this sample at three temperatures. The curves behavior was similar to the results in Figure 4. It was obviously seen from Figure 6 that the maximum absorption capacity (28.64 wt%) was much higher than that (11.33 wt%) of the  $\text{Li}_4\text{SiO}_4$  with AS at 600°C at 200 min. In order to analyze this reason, the experimental data were also fitted to the double exponential model, the results are shown on Table 3. As shown in Table 3, the ratio of  $k_1$  and  $k_2$  is more than 15, indicating that diffusion is also the limiting step. Following the same procedure, these data were fitted according to the Arrhenius theory (Figure 7). It is found that the results were better than those of the first data. The activation energies for chemisorption process and diffusion process were estimated to be 78.500 and 20.439 kJ/mol, respectively. By comparing the activation energies of two different silicon sources, some significant results were obtained. Obviously, the activation energies of the chemisorption process and diffusion for the sample with AS were higher than those of the sample with DS, indicating that the sample with DS had the higher reactivity and the better diffusivity due to structural differences



**Figure 6** Isotherms of  $\text{Li}_4\text{SiO}_4$  materials with DS.

**Table 3** Kinetic parameters obtained from the experimental data fitted to a double exponential model for the sample with DS

$T$ (°C)	$k_1$ (1/s)	$k_2$ (1/s)	$R$
500	0.16376	0.01122	0.99937
550	0.31428	0.01059	0.99817
600	0.35881	0.01331	0.99516

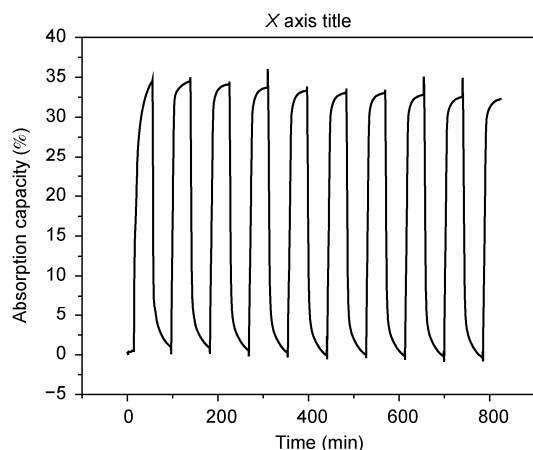


**Figure 7** Plots of  $\ln k$  versus  $1/T$  for chemisorption ( $k_1$ ) and diffusion ( $k_2$ ) on  $\text{Li}_4\text{SiO}_4$  with DS.

produced by the aluminum and other elements present on the diatomite [8,12]. The  $k_1/k_2$  ratio of the sample with DS was lower than that of the sample with AS, which showed the diffusion rate was relative quicker for the sample with DS. Seen from the above kinetic analysis for different silicon sources,  $\text{Li}_4\text{SiO}_4$  sorbents with AS and DS for  $\text{CO}_2$  absorption followed a double absorption mechanism [13].

## 2.4 Absorption-desorption performance measurement for DS

In order to investigate the cyclic absorption properties of the sample with DS, the absorption-desorption test was carried out at a fixed temperature (700°C) in a Netzsch thermogravimetric analyzer. During the test, a mixture gas (50 mL/min  $\text{N}_2$  and 50 mL/min  $\text{CO}_2$  for absorption and 100 mL/min  $\text{N}_2$  for desorption) were introduced into the system every 30 min. Figure 8 shows the absorption-desorption cycle number of  $\text{Li}_4\text{SiO}_4$  sorbents with DS. As shown in Figure 8, with increasing cycle number, the absorption capacity decreased 2.35 wt% from the first cycle (34.62 wt%) to the 10th cycle (32.27 wt%). This is probably because  $\text{Li}_4\text{SiO}_4$  sorbents with DS have particular structure, which refrained  $\text{Li}_4\text{SiO}_4$  sorbents from sintering in multinumber cycles. Compared with the lithium-based sorbents prepared by Marin et al. [14], the resultant  $\text{Li}_4\text{SiO}_4$  sorbents have the higher  $\text{CO}_2$  absorption capacity and better cyclic properties.



**Figure 8** Absorption-desorption performance of the  $\text{Li}_4\text{SiO}_4$  with DS.

Therefore, the resultant  $\text{Li}_4\text{SiO}_4$  sorbents with DS should have a potential application prospect for high temperature  $\text{CO}_2$  capture.

### 3 Conclusions

Novel  $\text{Li}_4\text{SiO}_4$  sorbents from diatomite for high temperature  $\text{CO}_2$  capture were prepared at low preparation cost. Effect of different silicon sources on  $\text{CO}_2$  absorption capacity was investigated by analyzing the kinetic characteristics. The following conclusions were obtained:

(1) The sample with DS had higher absorption capacity and absorption rate than that with AS at the same retaining time. The maximum absorption capacity of the sample with DS reached 28.62 wt%, being 78% of the theoretical absorption capacity.

(2) Some kinetic information about the  $\text{CO}_2$  absorption was obtained according to the double exponential model and the Arrhenius equation. The lower activation energies of the sample with DS for the chemisorption process and diffusion process were resulted from structural differences produced by the aluminum and other elements present on the diatomite.

(3) The  $\text{Li}_4\text{SiO}_4$  with DS had a good absorption-desorp-

tion performance. The absorption capacity only decreased 2.35 wt% from the first cycle (34.62 wt%) to the 10th cycle (32.27 wt%).

*This work was supported by the National Natural Science Foundation of China (51104075, 50963004 and 31160146) and the Natural Science Fund of Yunnan Province (2008B033M).*

- 1 Mavroudi M, Kaldis S P, Sakellariopoulos G P. Reduction of  $\text{CO}_2$  emissions by a membrane contacting process. *Fuel*, 2003, 82: 2153–2159
- 2 Park S W, Choi B S, Kim S S, et al. Mass transfer of carbon dioxide in aqueous polyacrylamide solution with methyldiethanolamine. *Korean J Chem Eng*, 2004, 21: 1205–1211
- 3 Choi W K, Kwon T I, Yeo Y K, et al. Optimal operation of the pressure swing adsorption (PSA) process for  $\text{CO}_2$  recovery. *Korean J Chem Eng*, 2003, 20: 617–623
- 4 Wilson M, Tontiwachwuthikul P, Chakma A, et al. Test results from a  $\text{CO}_2$  extraction pilot plant at boundary dam coal-fired power station. *Energy*, 2004, 29: 1259–1267
- 5 Mosqueda H A, Vazquez C, Bosch P, et al. Chemical sorption of carbon dioxide on lithium oxide. *Chem Mater*, 2006, 18: 2307–2310
- 6 Pfeiffer H, Bosch P. Thermal stability and high-temperature carbon dioxide sorption on hexa-lithium zirconate ( $\text{Li}_6\text{Zr}_2\text{O}_7$ ). *Chem Mater*, 2005, 17: 1704–1710
- 7 Pfeiffer H, Lima E, Bosch P. Lithium-sodium metazirconate solid solutions,  $\text{Li}_{2-x}\text{Na}_x\text{ZrO}_3$  ( $0 \leq x \leq 2$ ), a hierarchical architecture. *Chem Mater*, 2006, 18: 2642–2647
- 8 Gauer C, Heschel W. Doped lithium orthosilicate for absorption of carbon dioxide. *J Mater Sci*, 2006, 41: 2405–2409
- 9 Essaki K, Nakagawa K, Kato M, et al.  $\text{CO}_2$  absorption by lithium silicate at room temperature. *J Chem Eng Jpn*, 2004, 37: 772–777
- 10 Venegas M J, Israel E F, Escamilla R, et al. Kinetic and reaction mechanism of  $\text{CO}_2$  sorption on  $\text{Li}_4\text{SiO}_4$ : Study of the particle size effect. *Ind Eng Chem Res*, 2007, 46: 2407–2412
- 11 Rendon T A, Madrid J C, Pfeiffer H. Thermochemical capture of carbon dioxide on lithium aluminates ( $\text{LiAlO}_2$  and  $\text{Li}_5\text{AlO}_4$ ): A new option for the  $\text{CO}_2$  absorption. *J Phys Chem A*, 2009, 113: 6919–6923
- 12 Enriquez V, Mayra Y, Gonzalez G, et al. Synthesis and  $\text{CO}_2$  capture evaluation of  $\text{Li}_{2-x}\text{K}_x\text{ZrO}_3$  solid solutions and crystal structure of a new lithium potassium zirconate phase. *J Solid State Chem*, 2007, 180: 2485–2492
- 13 Palacios-Romero L M, Pfeiffer H. Lithium cuprate ( $\text{Li}_2\text{CuO}_2$ ): A new possible ceramic material for  $\text{CO}_2$  chemisorption. *Chem Lett*, 2008, 37: 862–863
- 14 Marin M O, Drage T C, Maroto-Valer M M. Novel lithium-based sorbents from fly ashes for  $\text{CO}_2$  capture at high temperatures. *Int J Greenh Gas Con*, 2010, 4: 623–629

**Open Access** This article is distributed under the terms of the Creative Commons Attribution License which permits any use, distribution, and reproduction in any medium, provided the original author(s) and source are credited.